



THE OHIO STATE UNIVERSITY

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# Optimization of Palladium Promoted Transition Metal Catalysts for Lean Methane Oxidation

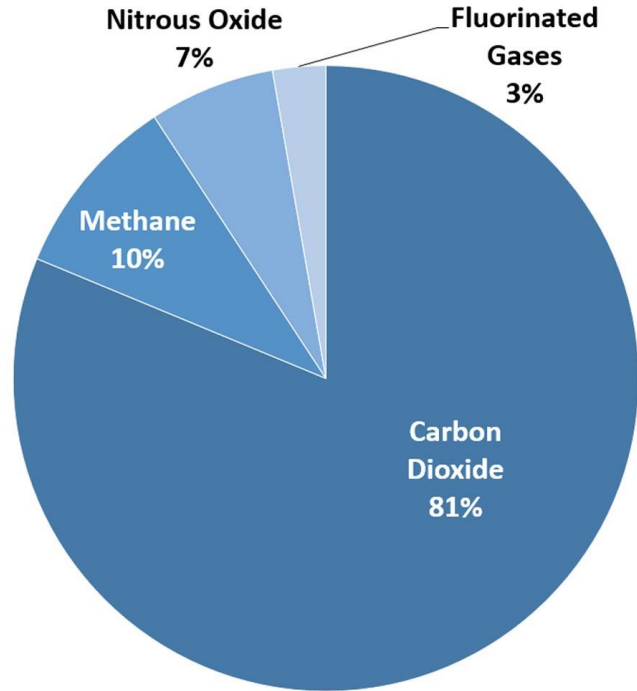
Brian Wynne, Deeksha Jain, Seval Gunduz, Umit Ozkan



# Introduction



Overview of Greenhouse Gas Emissions in 2018

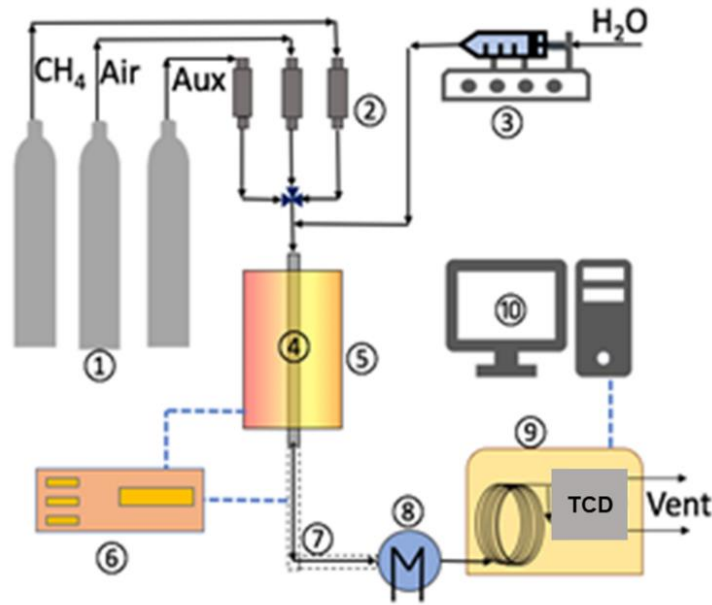


U.S. Environmental Protection Agency (2020). Inventory of U.S. Greenhouse Gas Emissions and Sinks: 1990-2018

## Motivation: Greenhouse Gases

- $\text{CO}_2$  appears to have the highest contribution to the global warming
- However, methane ( $\text{CH}_4$ ) global warming potential (GWP) is 25 times that of  $\text{CO}_2$  [2]
- Coal mining represents almost 10% of the United States methane emissions

Figure 1: Major greenhouse gases [1]



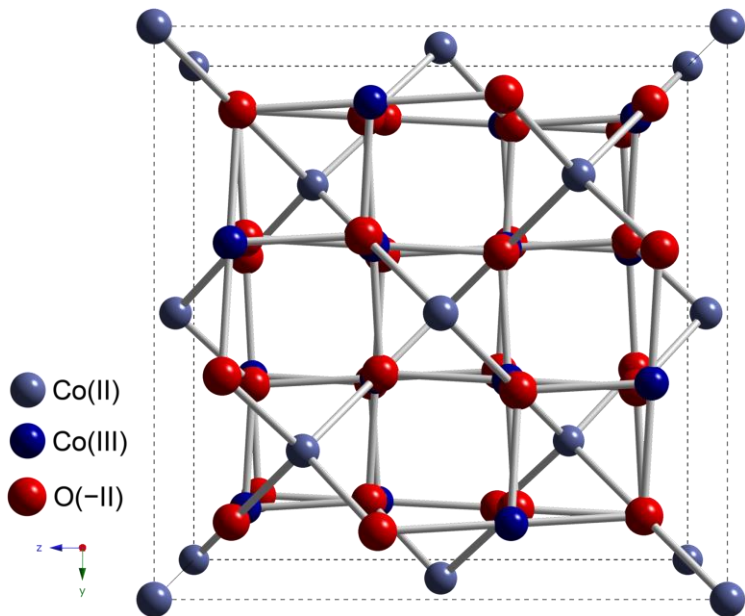
- (1) Gas Cylinders
- (2) Mass Flow Controllers
- (3) Syringe Pump/Bubbler
- (4) Packed Bed Reactor
- (5) Furnace
- (6) Temperature Controller
- (7) Heated Gas Lines
- (8) Water Condenser/PermaPure
- (9) Gas Chromatograph
- (10) Data Acquisition for GC

## Background: Methane Mitigation

- Ventilation systems ensure the safety of workers, but ventilation air methane (VAM) is released to the atmosphere
- Two approaches to VAM mitigation:
  - Ancillary
  - Principal
- Catalytic flow reversal reactor
  - Lower operating temperatures
  - Eliminating  $\text{NO}_x$  emission

Figure 2: Catalytic activity test system [3]

## Background: Catalyst Selection



- Noble metals typically used due to high activity
- Palladium (Pd) and Platinum (Pt) for methane oxidation
  - Pd can form highly active PdO [5]
- Downsides to noble metals
  - High cost
  - Scarcity
  - Sensitivity to water
- Transition metals as alternatives
  - Cobalt (II,III) oxide:  $\text{Co}_3\text{O}_4$

Figure 3: Unit cell of  $\text{Co}_3\text{O}_4$  [6]



# Methods

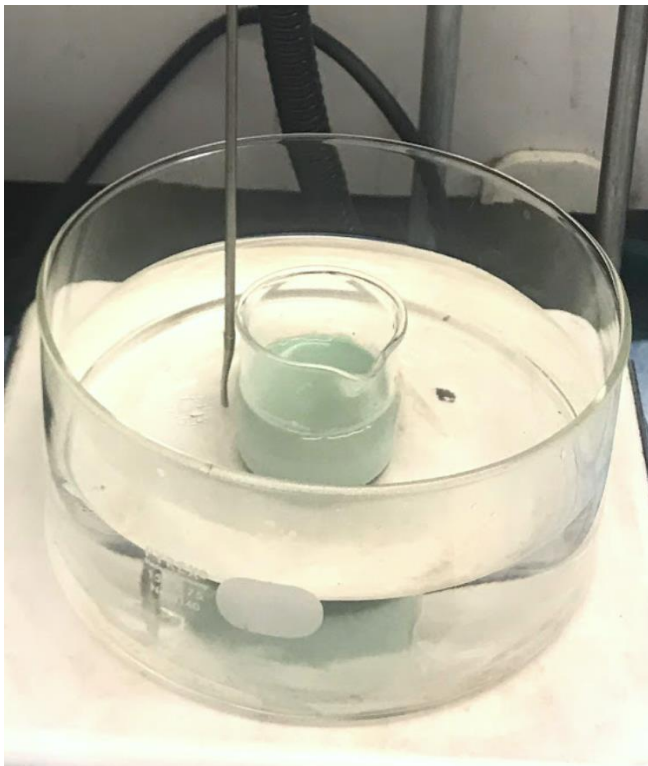


Figure 4: Wet impregnation mixture

## Catalyst Synthesis

- Wetness impregnation (WI) technique
- Cobalt on metal oxide support materials
  - alumina ( $\text{Al}_2\text{O}_3$ ), silica ( $\text{SiO}_2$ ), zirconia ( $\text{ZrO}_2$ ) and ceria ( $\text{CeO}_2$ )
- Solvent evaporation and dried in oven
- Calcined with air at  $400^\circ\text{C}$  for 3 hours



## Catalyst Characterization

- X-ray diffraction (XRD) technique
- Detects intensity of scattered x-rays
- Characteristic peaks for each compound
- Bragg's Law:

$$n \lambda = 2 d \sin(\theta)$$

Figure 5: X-ray diffraction instrument



## Temperature programmed reduction

- Reducibility of the  $\text{Co}_3\text{O}_4$  active sites
- Oxygen mobility of catalysts
- 5% hydrogen in nitrogen
- 1000°C for 1 hour
- Gas outlet to mass spectrometer

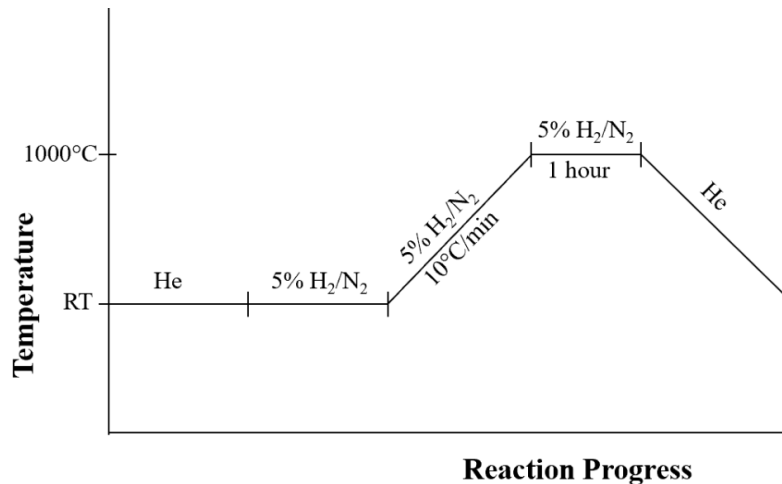


Figure 6: TPR Heating Scheme

## Activity Tests

- Packed bed reactor system
  - 50mg of catalyst, bed height of 0.4cm
- Activity screening to find best catalyst
- Methane conversion tests
  - Promoter comparison
  - Water stability

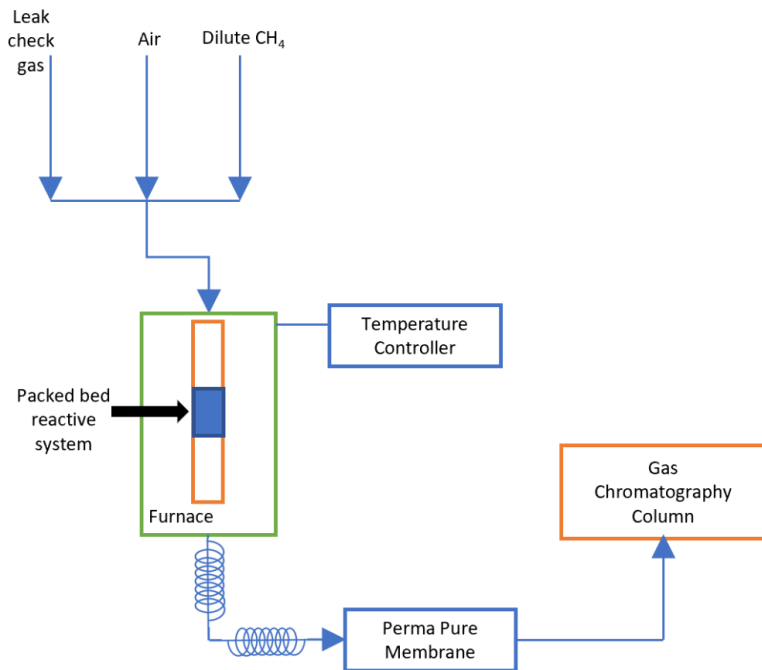
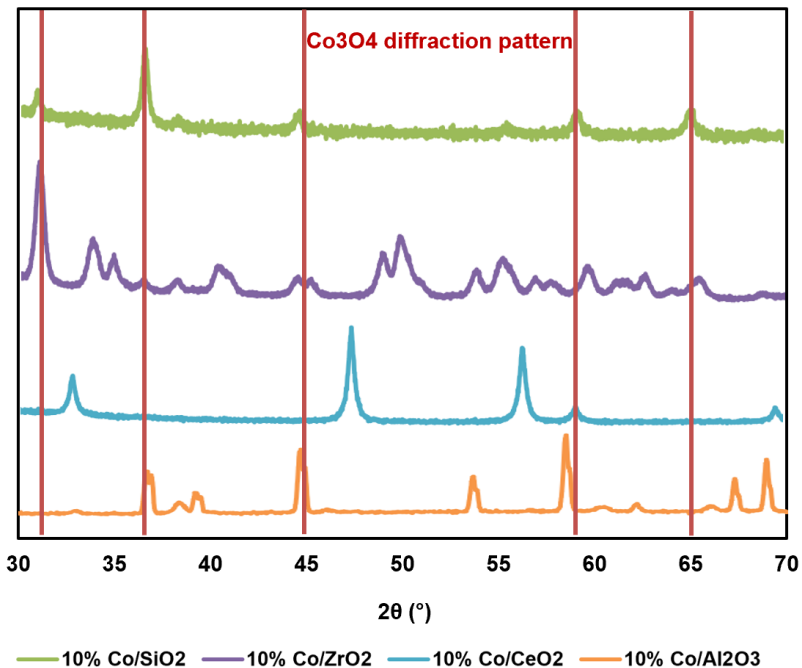


Figure 7: Activity Test Setup



# Results

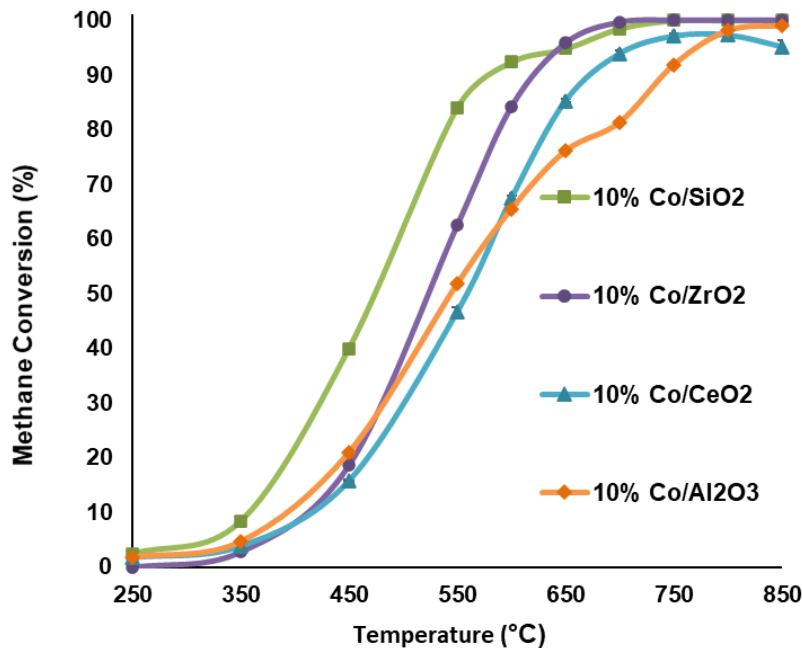
## XRD Catalyst Characterization



- Investigate crystalline structures
- Diffraction pattern of synthesized catalysts
- Red bars show Co<sub>3</sub>O<sub>4</sub> diffraction pattern [4]
- Indicates that Co has been oxidized to Co<sub>3</sub>O<sub>4</sub> during calcination

Figure 8: XRD Patterns

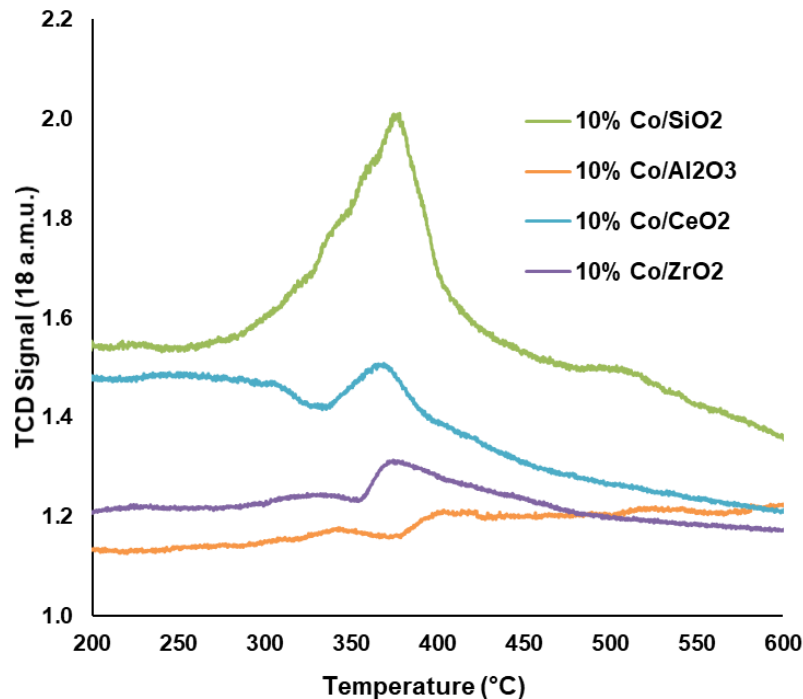
## Activity Tests



- 10% Co/SiO<sub>2</sub> better at lower temperatures
- At higher temperatures, 10% Co/ZrO<sub>2</sub> and 10% Co/SiO<sub>2</sub> had similar activity
- Unexpected high activity of 10% Co/SiO<sub>2</sub>
  - High surface area (~300 m<sup>2</sup>/g)
  - Lower GHSV (gas hourly space velocity) value due to lower density

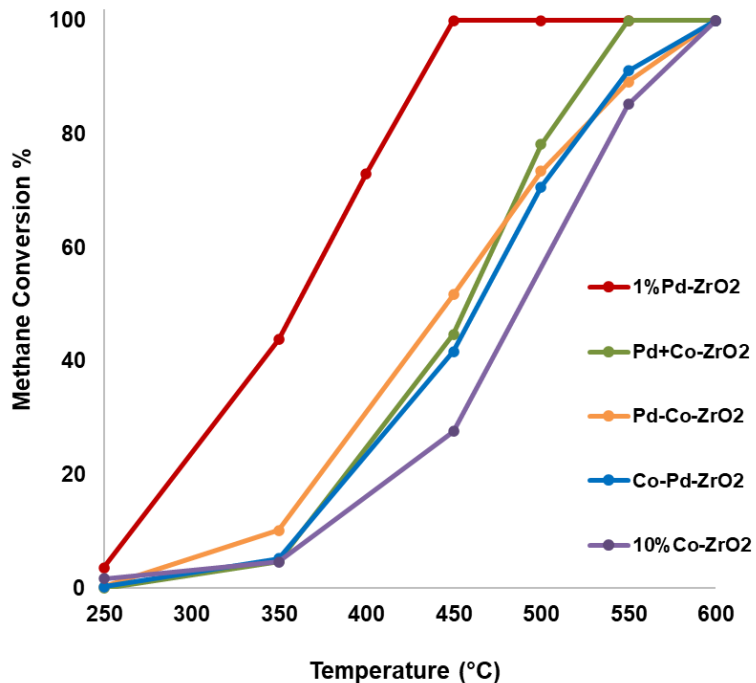
Figure 9: Lean methane oxidation activity

## Temperature programmed reduction (TPR)



- Thermal conductivity detector (TCD)
- Reducibility of Co<sub>3</sub>O<sub>4</sub> on different support materials
- Areas under curves:
  - 10% Co/SiO<sub>2</sub> >> 10% Co/ZrO<sub>2</sub>
- Co<sub>3</sub>O<sub>4</sub> phase reduced to CoO and Co:
  - Greatest in 10% Co/SiO<sub>2</sub>
  - Least in 10% Co/ZrO<sub>2</sub>
- 10% Co/ZrO<sub>2</sub> chosen due to activity and resistance to reduction of Co<sub>3</sub>O<sub>4</sub> phase

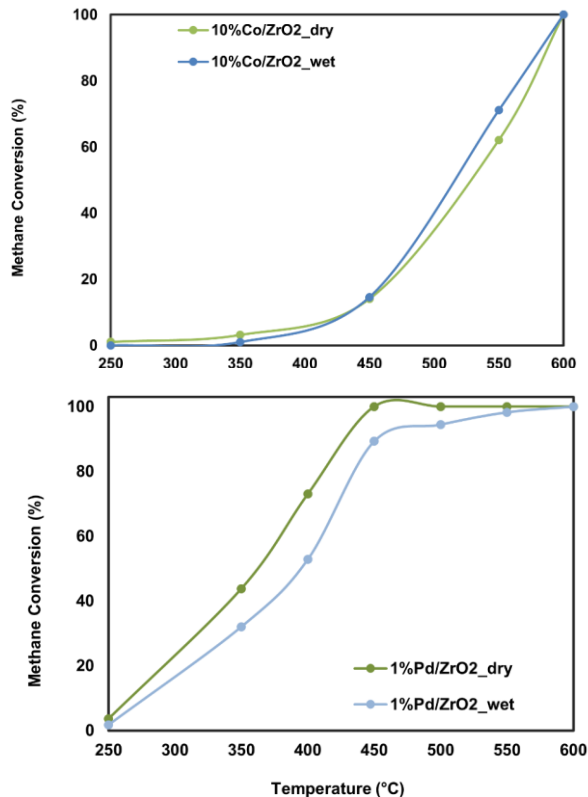
Figure 10: TPR of 10% Co/SiO<sub>2</sub>, Al<sub>2</sub>O<sub>3</sub>, CeO<sub>2</sub>, and ZrO<sub>2</sub>



## Promoter Addition

- Palladium as promoter, Pd/PdO active phase
- Comparison of promoter and order of synthesis
- 3 varied orders showed differences due to accessibility of Pd on catalyst surface
- Pd-Co-ZrO<sub>2</sub> was deactivated at higher temperatures due to H<sub>2</sub>O

Figure 11: TPR of 10% Co/SiO<sub>2</sub>, Al<sub>2</sub>O<sub>3</sub>, CeO<sub>2</sub>, and ZrO<sub>2</sub>



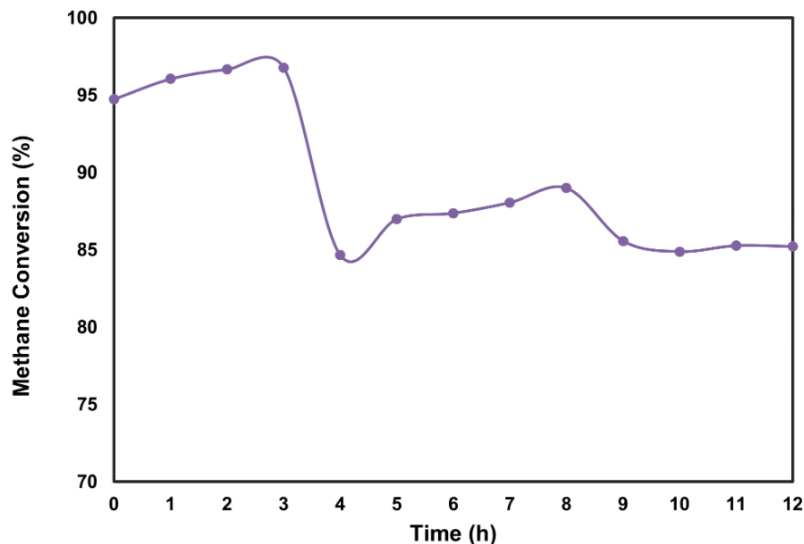
## Wet Activity Tests of Co and Pd Catalysts

- Catalytic activity test with 3% water in the feed
- Cobalt catalyst not affected
- Palladium catalyst showed inhibition with water
- Pd activity higher overall, but Co preferred because no deactivation

Figure 12: Activity tests in the presence and absence of water



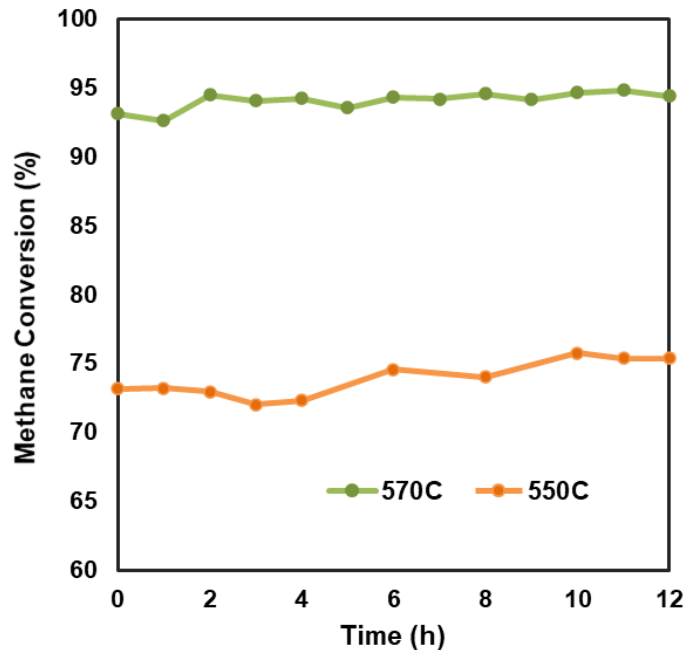
## Long-Term Stability Test: Pd



- Testing 1% Pd/ZrO<sub>2</sub> catalyst
  - In presence of 3% water
- Showed instability of palladium catalyst over time in presence of water
  - Over the long-term test
- Not recommended as catalyst deactivates

Figure 13: Wet methane oxidation of 10% Co/ZrO<sub>2</sub>

## Long-Term Stability Test: Co

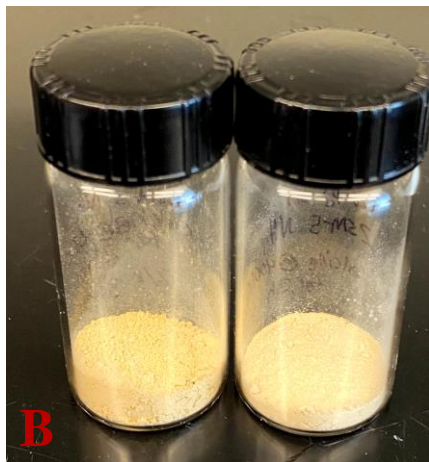
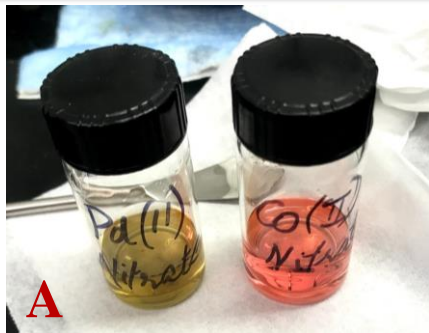


- Testing the 10% Co/ZrO<sub>2</sub> catalyst in the presence of water
- Activity test performed at 550°C and 570°C for 12 h
- Showed that the Co/ZrO<sub>2</sub> catalyst is highly stable catalyst under reaction conditions:
  - Operated at two different methane conversion conditions
  - Resistant to presence of water

Figure 14: Wet methane oxidation of 10% Co/ZrO<sub>2</sub>



# Conclusion



## Summary

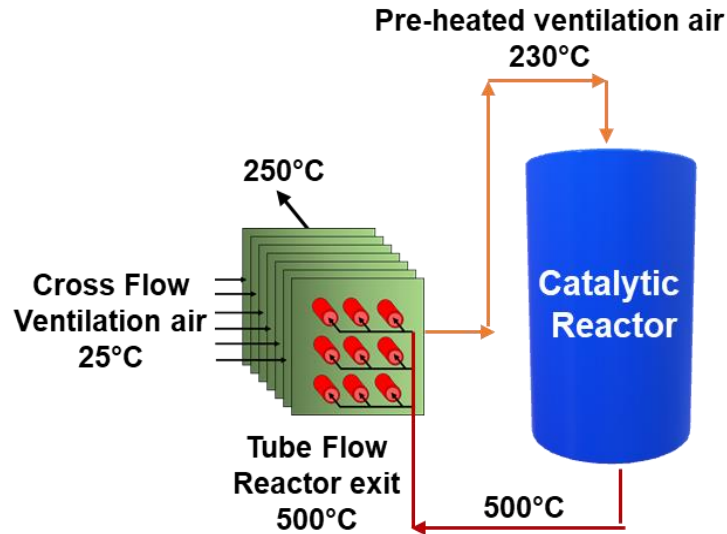
- Catalytic mitigation of coal-mine VAM
- Cobalt catalysts synthesized on different metal oxide supports
- Pd promotion showed similar to Pd based
- Co-based showed resistance to presence of water vapor
- Demonstrated the potential Co/ZrO<sub>2</sub> catalyst
- Co-based more economically feasible than Pd-based

Figure 15: Catalysts at the A. beginning and B. end of synthesis



# Future Work

## Commercialization



- Catalytic oxidation reduces the auto-ignition temperature and  $\text{NO}_x$  emission
- Balances on system show exhaust stream can be used for pre-heating
- Further pilot-scale research needed:
  - Fluctuations in pressure and temperature
  - Verify scaled-up parameters
  - Effect on  $\text{NO}_x$  emission

Figure 16: Commercial Design for Catalytic Oxidation of VAM [3]



- [1] *Overview of Greenhouse Gases*. 8 Sept. 2020, [www.epa.gov/ghgemissions/overview-greenhouse-gases](http://www.epa.gov/ghgemissions/overview-greenhouse-gases).
- [2] Forster, P., V. Ramaswamy, P. Artaxo, T. Berntsen, R. Betts, D. Fahey, J. Haywood, J. Lean, D. Lowe, G. Myhre, J. Nganga, R. Prinn, G. Raga, M. Schulz & R. Van Dorland (2008): *Changes in Atmospheric Constituents and in Radiative Forcing*. *Climate Change 2007: The Physical Science Basis*. Contribution of Working Group I to the Fourth Assessment Report of the IPCC, S. Solomon et al. (eds.), Cambridge University Press, Cambridge, UK, Chapter 2  
<http://www.cambridge.org/catalogue/catalogue.asp?isbn=9780521705967>
- [3] Ozkan, U., S. Gunduz, D. Jain, B. Wynne. "Catalytic Combustion of Methane Emitted from Coal Mine Ventilation Air Systems." OCRC Agreement Number: R-17-14.
- [4] Kumari, T. Sri Devi, T. Prem Kumar, and A. Manuel Stephan. "Lithium insertion behavior of nanoscopic Co<sub>3</sub>O<sub>4</sub> prepared with avian egg membrane as a template." *Bull. Korean Chem. Soc* 32.4 (2011): 1205.
- [5] Baldwin, T. R., and R. Burch. "Catalytic combustion of methane over supported palladium catalysts: I. Alumina supported catalysts." *Applied catalysis* 66.1 (1990): 337-358.
- [6] Mills, B. Ball-and-stick model of the unit cell of cobalt(II,III) oxide, Co<sub>3</sub>O<sub>4</sub>. Colour code: Cobalt(II), CoII: lighter blue Cobalt(III), CoIII: darker blue Oxygen, O: red Crystal structure from J. Magn. Magn. Mater. (2006) 300, 300–305 Image generated in CrystalMaker 8.2.



# Questions?

## Recap:

- Catalytic mitigation of coal-mine VAM
- Cobalt catalysts synthesized on different metal oxide supports
- Pd promotion showed similar to Pd based
- Co-based showed resistance to presence of water vapor
- Demonstrated the potential Co/ZrO<sub>2</sub> catalyst
- Co-based more economically feasible than Pd-based